

REINHOLD ENVIRONMENTAL Ltd.



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Presentation**

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# EVALUATING DSI PERFORMANCE AND BALANCE OF PLANT EFFECTS

2019 Reinhold Conference

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# PRESENTATION OVERVIEW

- Presentation
  - Audience is Panel
  - Discussion Encouraged
  - Scope for New & Experienced
- Q & A/ Discussion

## Background & Perspective

- 30+ Years of Utility Power Plant Experience
- 20 Years of SO<sub>3</sub> Mitigation Experience
- Testing, System Design & Construction, O&M
  
- Designed and/or Operated Systems Using Most Available Reagents
  - Calcium (Hydrated Lime, Limestone, Cao)
  - Sodium (Trona, Sodium Bicarbonate, SBS) (Wet & Dry)
  - Magnesium (Mag Hydroxide (Wet & Dry), Magnesium Sulfate (Wet))
  
- Various Injection Locations
  - Wet & Dry
  - Furnace to FGD Inlet
  - Coal Additives
  
- Integrated/ Holistic Approach Critical
- Experience varies significantly though fundamental principles are the same
  
- Past experience critical but past conclusions can be misleading

## GENERAL DSI EVALUATION DISCUSSION

- DSI Performance Evaluation
  - Improve Pollutant Capture Effectiveness
    - SO<sub>3</sub>/SO<sub>2</sub>/HCl
    - Se/As?
  - Hg PAC/Capture support
  - Sorbent Comparisons
  - Equipment Comparisons
- Balance of Plant Effects/ Impacts Assessment
  - Air Heater Fouling Reduction
  - SCR Turndown/ MOT Reduction
  - Minimize Fly Ash impacts



## IMPORTANCE OF WELL THOUGHT OUT EVALUATIONS

- Often significant decisions & costs are at stake
- Inaccurate / Incomplete Data or Wrong Conclusions can be very, very costly!!
  - Minimum may require re-testing
  - Worse could lead to wrong decisions regarding compliance strategies
  - Could Lead to Costly Capital and Operating Decisions
  - Could lead to significant BOP Impacts
- Want to Maximize Useful Data @ Least Cost

## DSI TRIAL PLANNING – GENERAL CONSIDERATIONS

- Iterative process
- Cost
- Practicality
- Data Prioritization
- Whole Unit vs Part unit DSI
- Unit Conditions
- Input from station - Critical
  - More complex >>more input & planning, meetings required

## UNDERSTAND CHALLENGES OF SO<sub>3</sub> MEASUREMENT

- SO<sub>3</sub> Measurement is Not an Exact Science!
  - Controlled Condensate is currently the 'Gold Standard' but can vary significantly between testers
    - Some Experts say best precision is +/- 0.5 to 1 ppm not 0.01 ppm as is often shown on test reports
  - Acid Dewpoint Measurement & SO<sub>3</sub> Correlation
  - Sorbent Traps
  - Newer SO<sub>3</sub> CEMS
- All have limitations and significant potential biases
- Impacted by sorbent in gas stream
- Impacted by sampling location
- Impacted by other constituents (eg HCl, etc)
- Impacted by sampling technique

# VISIBLE PLUME

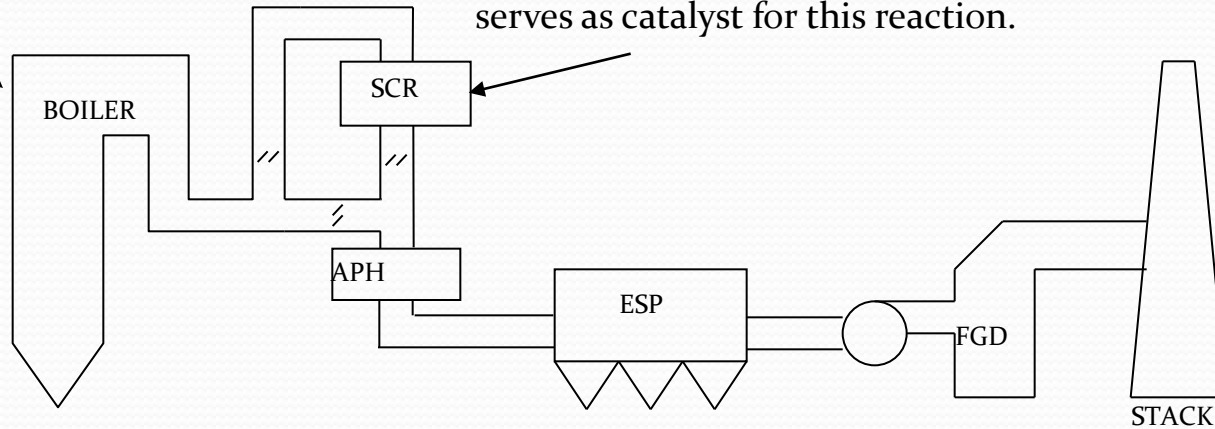


- Opacity due to small quantities of  $\text{H}_2\text{SO}_4$  (Sulfuric Acid) Aerosols in Flue Gas
- Aerosols produced from  $\text{SO}_3$  in flue gas when quenched in Absorber Mods

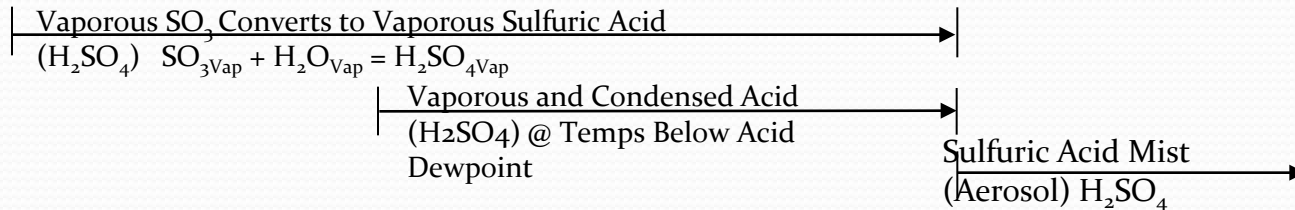
# HOW SO<sub>3</sub> IS FORMED

In Boiler approx 1% of SO<sub>2</sub> oxidizes to form SO<sub>3</sub>

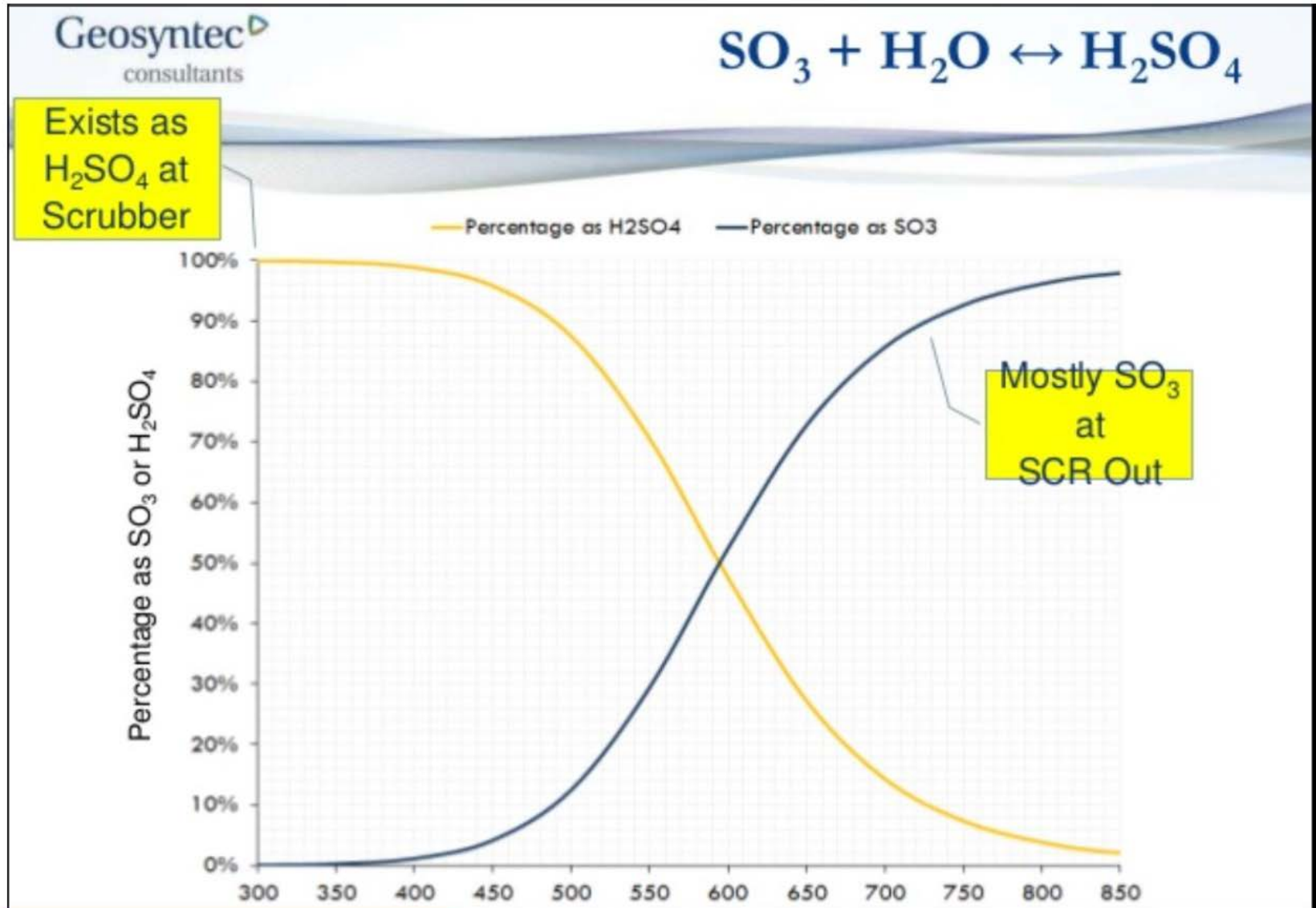
In SCR additional 0.75% -to-1.5% of SO<sub>2</sub> oxidizes to form SO<sub>3</sub>. Vanadium in SCR serves as catalyst for this reaction.



## Physical Forms of SO<sub>3</sub>



# SO<sub>3</sub> vs H<sub>2</sub>SO<sub>4</sub> Measurement Considerations



## DSI EVALUATION PLANNING

### Determine Objectives

- Primary Goals?
  - Quantify/ Confirm Performance
  - Determine Sorbent Choice
  - Determine BOP Impacts
- Secondary Goals? - THINK AHEAD, THINK INTEGRATED
  - Corrosion Mitigation
  - Reduce APH Pluggage
  - Secondary acid gas mitigation
  - SCR Turndown
  - Other Beneficial BOP Impacts?

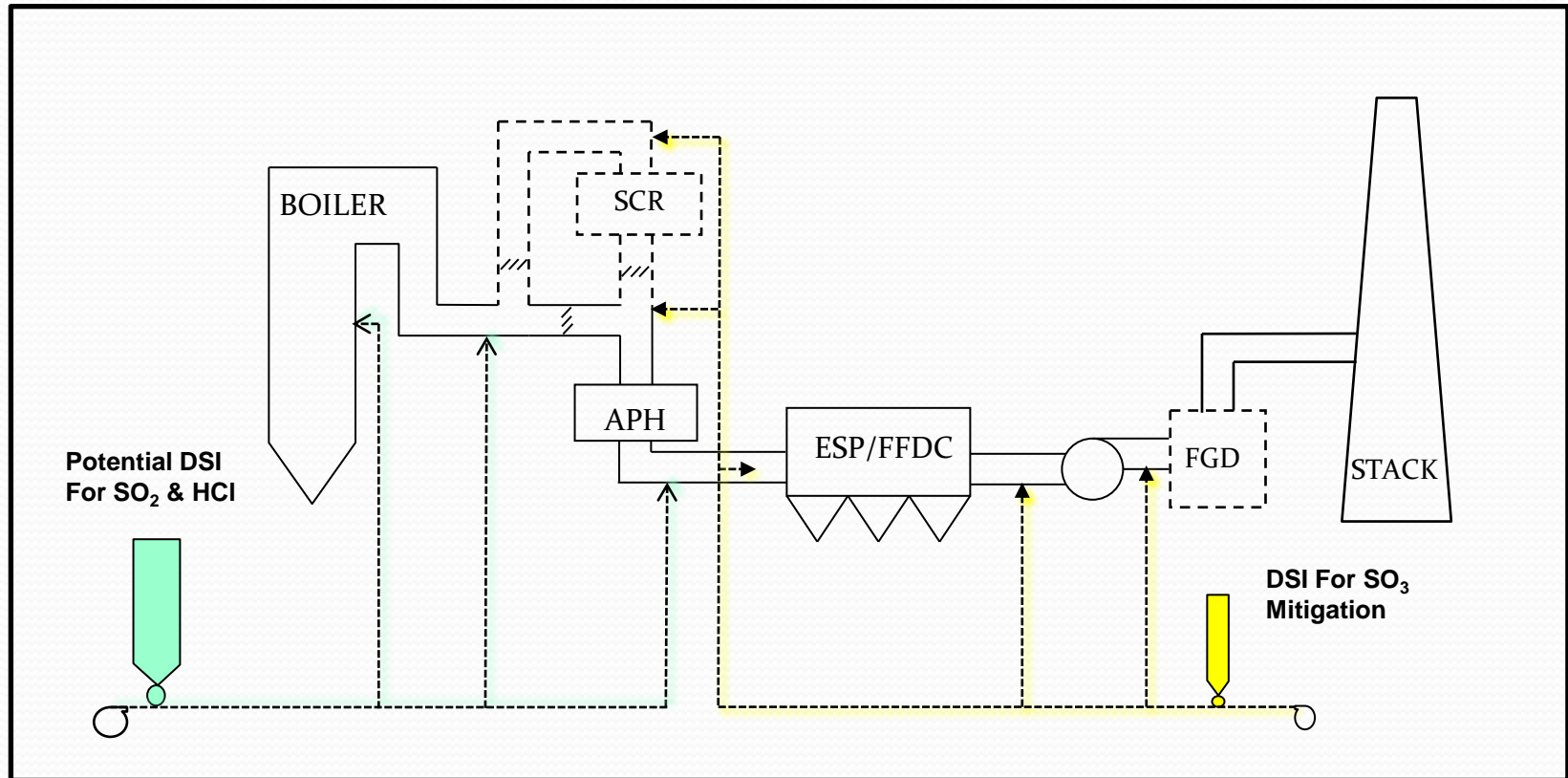
Screening trial –vs-Longer term trial

## DSI TRIAL PLANNING

### Limitations & Constraints

- Time Constraints
- Cost
- Unit Configuration
  - Current Equip
  - Inject Location Possibilities
    - Residence Time, Etc
- Baseline
- Conditions must be carefully considered
  - Daily ambient temperature effects
  - SCR 'morning sickness'
  - Daily boiler slag building & shedding overnight
- Fuel
  - Type & Variability
  - Delivery Issues

# POTENTIAL DSI INJECTION LOCATIONS



# DSI TRIAL PLANNING - CONSIDERATIONS

## Test System Design

- Reagent Type(s)
- Expected Feed & Turndown
- Expected/ Potential Trial Duration
- Utility Design & Constructed
- Vendor Rental System

# Plant Site Planning & Preparation

## Sampling Location - Critical

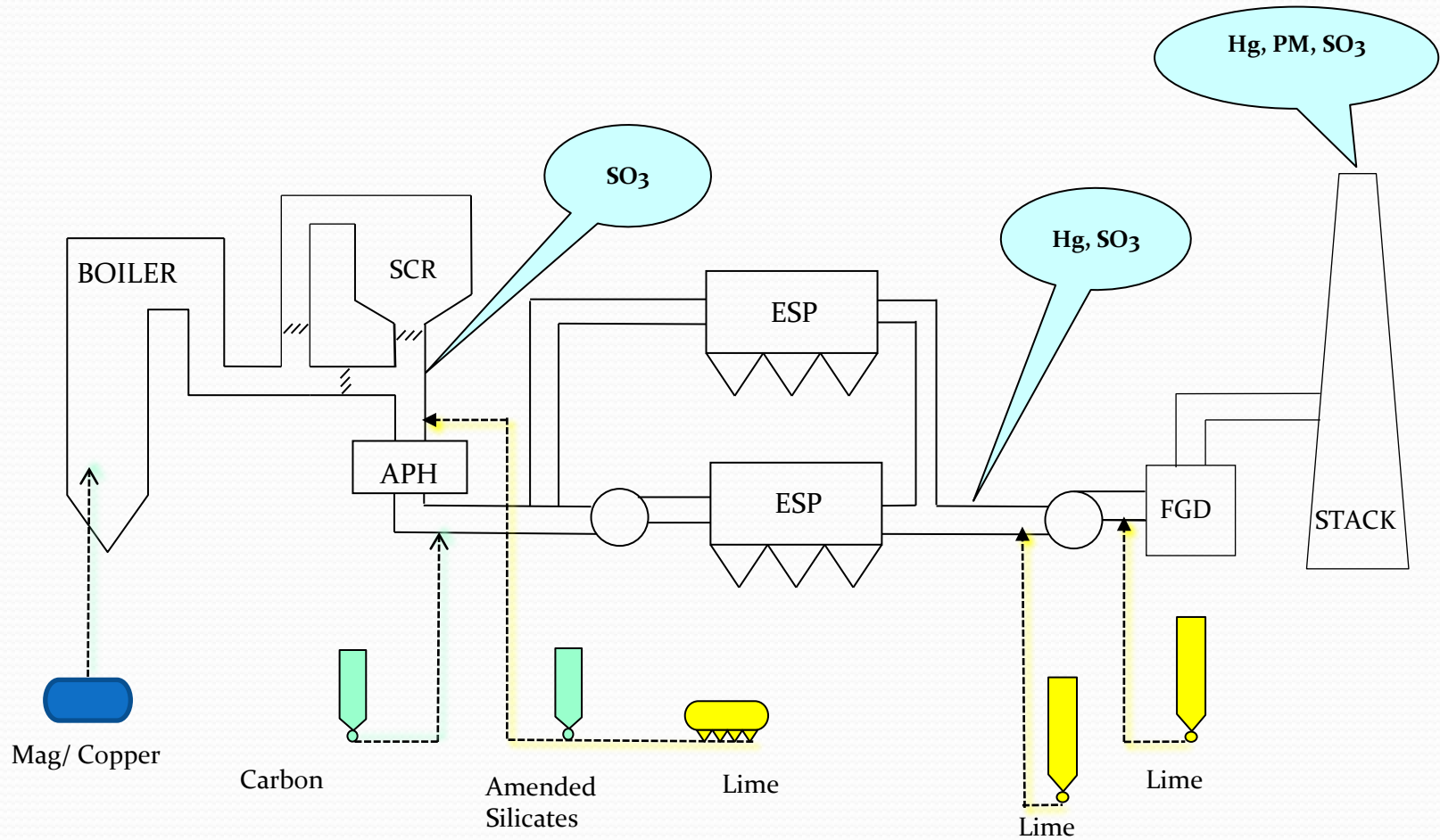
- Stratification
- Gas/ Aerosol State
- Air Inleakage
- Sorbent & Dust Loading

## Injection Location – Critical

- Temp
- Gas Flow Pattern

## Ports & Internal Obstructions – Verify

# COMPLEX TEST LAYOUT



# DSI TRIAL PLANNING - CONSIDERATIONS

## Sampling & Data Collection

- Selection of Gas Sampling Firm
- Continuous (CEMS) vs. Periodic Sampling
- 'Steady State' determination
- Data Repeatability
- Ash & Gypsum Sampling

# DSI TRIAL CONTINGENCY PLANNING

## Potential Trial Problems

- DSI Equip Issues
  - Feed Problems
  - Dispersion
  - Reagent Delivery
  
- Sampling Issues
  - Sampling Equip Problems
  - Unreliable Data
  
- Plant Issues
  - Unit Load Variability
  - Other Plant Systems
  - Coal Consistency

Know Most important objectives & adjust accordingly

## DSI TRIAL PLANNING & EXECUTION

### Unit Conditions

- Full Load vs. Cycling
- Coal Loading Schedule
- Furnace Conditions
  - NO<sub>x</sub> Set Point
  - Sootblowing Schedule

### AQCS Conditions

- SCR Operation
- ESP & FFDC Condition
  - Rapping Schedule
  - Ash Sampling
  - Bag Cleaning schedule
  - Ash Sampling
    - Hopper Evacuation
- FGD Conditions

## DSI TRIAL EXECUTION & DATA COLLECTION

### Prelim-Testing

- DSI System
- Check CEMS
- Determine/ confirm minimum *acceptable* conditioning time

### Coordinate and Follow Test Plan

### Initial Results Review

- Daily Review of results
- Compare to expected

## DSI TRIAL – EVALUATION OF BOP IMPACTS

Impacts determined in part by:

- Reagent
- Feed rate
- Injection Location
- Residence Time
- Dispersion Pattern
- Fuel
- Existing Equipment & Systems Issues
- Ash Disposal
- Unit Cycling

# EVALUATION OF POSSIBLE BOP IMPACTS

## SORBENT IMPACTS BASED ON INJECTION LOCATION

- Pre-FGD
  - PM Emissions
  - ME Pluggage
  - Duct Layout
- Pre ID Fan
  - Fan Deposits
  - Erosion
- Pre ESP
  - Resistivity
  - Mass Loading
  - Ash Handling
  - Ash Disposal
- Pre APH
  - Hg Impacts
  - Pluggage Concern
- Pre SCR
  - Catalyst Impacts
  - Hg Impacts (HCl)
- Boiler
  - Pluggage
  - Deposits

## DSI TRIAL – EVALUATION OF BOP IMPACTS

- Many BOP Impacts take time to show
  - Allow sufficient time if necessary
- Many BOP impacts require inspections to confirm
  - Sooner is better
- Careful not to blame DSI for other root cause

## DSI TRIAL – EVALUATION OF BOP IMPACTS

- Poor Dispersion is often the cause of BOP problems
  - General sorbent overfeed
  - Localized sorbent overfeed
- Improved dispersion can reduce and possibly eliminate some BOP problems
- When comparing sorbents or injection system options make sure the existing system is cleaned and in good operating condition
  - Don't Assume problems cannot be fixed!

# HYDRATE DISPERSION



## EXAMPLE OF MISDIAGNOSED PROBLEM

Hydrate Deposits Typically Only A Problem With Moisture



## EXAMPLE OF CONSIDERATIONS FOR APH IMPACTS EVALUATION

- APH Fouling is typically due to condensation of  $H_2SO_4$  on element and ash surfaces and leads to sticky buildups
- SCR additions led to formation of ABS deeper in elements. Soot blowers typically can't reach
- Reducing  $SO_3$  Concentration has been shown repeatedly to reduce APH Fouling

# 2 LAYER AIR HTR w/ SCR & Increased NH3 Slip

GAS INLET TEMP = 700F

Plate = 660F

Plate = 640F

Plate = 620F

Plate = 600F

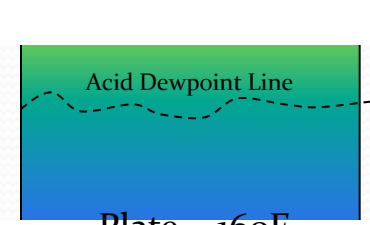
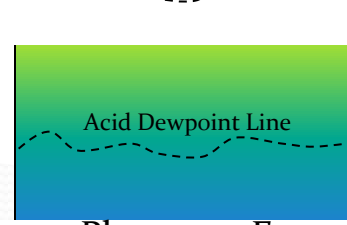
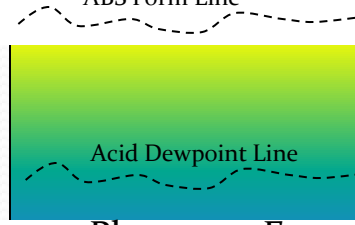
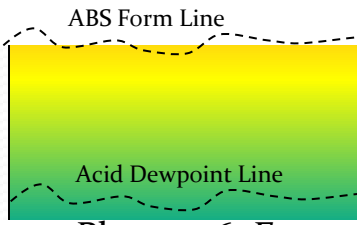
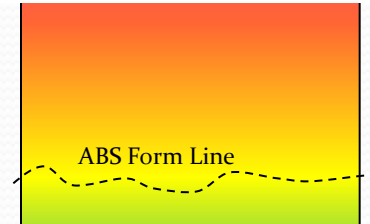
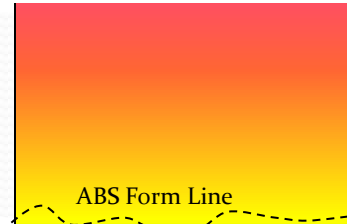
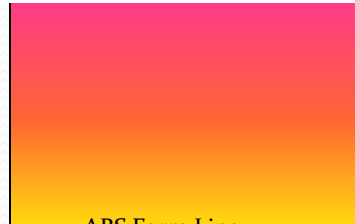


Plate = 260F

Plate = 230F

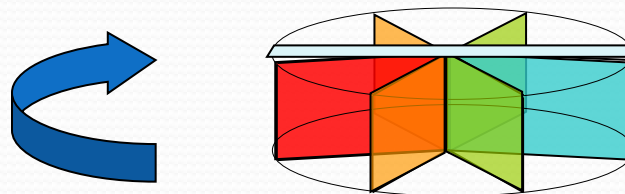
Plate = 190F

Plate = 160F

Hot Side Gas  
320 F

AVG GAS OUTLET TEMP = 290F

Cold Side Gas  
260 F



# AIR HTR w/ SCR & Increased NH3 Slip & Pre APH SO3 Mitigation

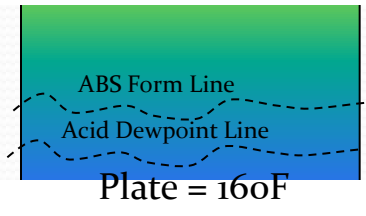
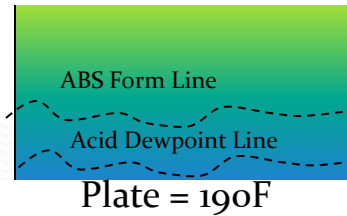
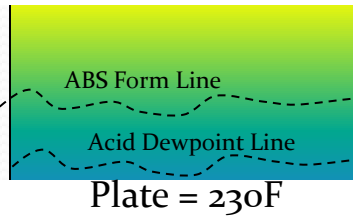
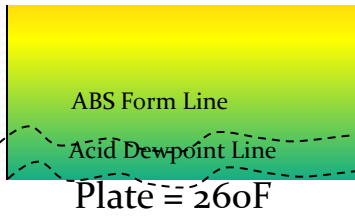
GAS INLET TEMP = 700F

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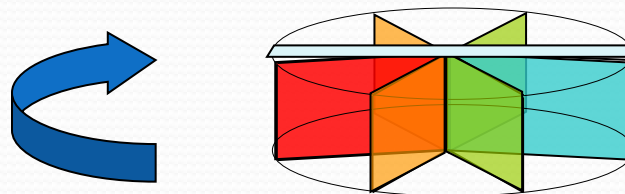
Plate = 600F



Hot Side Gas  
320 F

AVG GAS OUTLET TEMP = 290F

Cold Side Gas  
260 F



# EXAMPLE OF CONSIDERATIONS FOR APH IMPACTS EVALUATION

- Significant Potential for Fouling Reduction by reducing SO<sub>3</sub> Pre-APH.
- The question is what should the target be?
- Elimination of SO<sub>3</sub>/H<sub>2</sub>SO<sub>4</sub> will eliminate fouling
  - Can however lead to significant overinjection and BOP problems
- Another option is to find what SO<sub>3</sub> levels are actually needed to reduce fouling to levels that the soot blowers are capable of handling
  - Requires a careful evaluation of AHDP vs sorbent feeds and possibly of H<sub>2</sub>SO<sub>4</sub> Dewpoints or SO<sub>3</sub>

## EXAMPLE OF CONSIDERATIONS FOR APH IMPACTS EVALUATION

### Additional Considerations

- If station wants to consider lowering APH temps by changing APH elements:
  - Need to consider DP impacts
  - Will LPA be a problem?
  - Materials of construction
  - Can coatings be eliminated
  - How low can temps be taken?
- May need to test varying SAH inlet temps ahead of an outage incase probs occur
- Testing needs to be done in time for capital budgeting and material acquisition
- Next opportunity could be 4-7 years if miss chance to prove

## DSI TRIAL – COMPLETION

- Review Data Immediately
  - Does data make sense?
  - Were plant conditions varying enough to be problematic
- Determine if additional testing needed before removing Test Equipment if possible

## SUMMARY & CONCLUSION

- Planning is Critical to Success of Evaluations
- Know Objectives
  - Primary
  - Secondary
  - Potential Future Needs
- Understand Measurement Uncertainties
- Know Data Priority
- Expect Problems and Be Ready to Adjust
- Consult with Plant
- Consult with Experienced Personnel

## SUMMARY & CONCLUSION

- Be Practical
  - Consider limitations of station personnel
- Know the basis of “Targets”
  - Don’t expend disproportionate cost & effort trying to solve minor ‘problems’
- Understand Measurement Uncertainties

# Questions

